

Basics of Vacuum Technology

Unit: Pa = N/m² = J/m³

Unit		Pa or N/m²
bar		10 ⁵
mbar		100
atm	= 760 torr	1.01325 x 10 ⁵

Three states of residual gas

- d = typical distance between walls
- $\langle \lambda \rangle$ = average collision distance

Viscous state: $\langle \lambda \rangle < d/100$

- Collisions, energy transfer through collisions, viscous flow, diffusion

Intermediate state: $d/100 < \langle \lambda \rangle < d$

Molecular state: $d < \langle \lambda \rangle$

- Molecules collide with the walls, heat transfer from wall to wall with molecules, no viscosity

Vacuum regions

Vacuum region	Pa
Rough	$10^5 - 10^2$
Intermediate	$10^2 - 10^{-1}$
High	$10^{-1} - 10^{-4}$
Good high	$10^{-4} - 10^{-7}$
Ultra	$10^{-7} - 10^{-10}$
Good ultra	$10^{-10} -$

Vacuum region

Rough

Viscous

Intermediate

Changing to molecular

High

Mainly molecular

Good high

Molecular

Materials, tightness, baking
(150 – 400 °C)

Ultra

Surfaces stay clean

Materials critical, metal
seals, baking

Good ultra

Residual gas

- Initially air
- Rough vacuum: mainly air
- Intermediate vacuum: gas starts to get out from surfaces (outgassing)
- High vacuum: Mainly gases from surfaces, typically 70 – 90 % water
Gradually water decreases and CO + CO₂ increase
- Ultra vacuum: mainly Hydrogen
- Depends on Pump/pre-pump: most pumps pump easier heavy gases
- Nobel gases difficult to pump
- Principally residual gas is NOT thin air*

Note!

The composition of residual gas depends on

- how long time the vessel has been open
- how it was vented
- what molecules can have attached on the surface (e.g. humidity
-> water)
- possible leaks
- Etc.

Vacuum forces

$$F = P \cdot A$$

Practically “zero” pressure on the vacuum side and 1 atm on the pressure side.

- e.g. 10 cm x 10 cm square flange:

$$F = 1.013 \times 10^5 \text{ N} / \text{m}^2 \times (0.1\text{m})^2 = 1000\text{N}$$

This is important when designing vacuum vessels/chambers!

Some constants and equations

$$N_A = 6.02205 \cdot 10^{23} \text{ mol}^{-1} \quad \text{Avogadro constant}$$

1 mol ideal gas in NTP = 22.4 l

$$R = 8.3144 \text{ J/mol} \cdot K \quad \text{molar gas constant}$$

$$P \cdot V = n \cdot R \cdot T \quad \begin{array}{l} \text{Equation of state for} \\ \text{residual gas in terms of} \\ \text{moles} \end{array}$$

$$k = R / N_A = 1.3806 \cdot 10^{-23} \text{ J/K} \quad \text{Boltzmann constant}$$

$$P \cdot V = N \cdot k \cdot T \quad \begin{array}{l} \text{Equation of state for} \\ \text{residual gas in terms of} \\ \text{number of molecules} \end{array}$$

Number of gas molecules

One cubic-cm in NTP

$$N = \frac{P \cdot V}{k \cdot T} = \frac{10^5 \text{ N/m}^2 \cdot 10^{-6} \text{ m}^3}{1.38 \cdot 10^{-23} \text{ J/K} \cdot 293 \text{ K}} = 2.5 \cdot 10^{19}$$

$$10^{-7} \text{ mbar} = 10^{-5} \text{ Pa: } N = 2.5 \times 10^9 \quad (\text{molecules in cm}^3)$$

Energy in residual gas

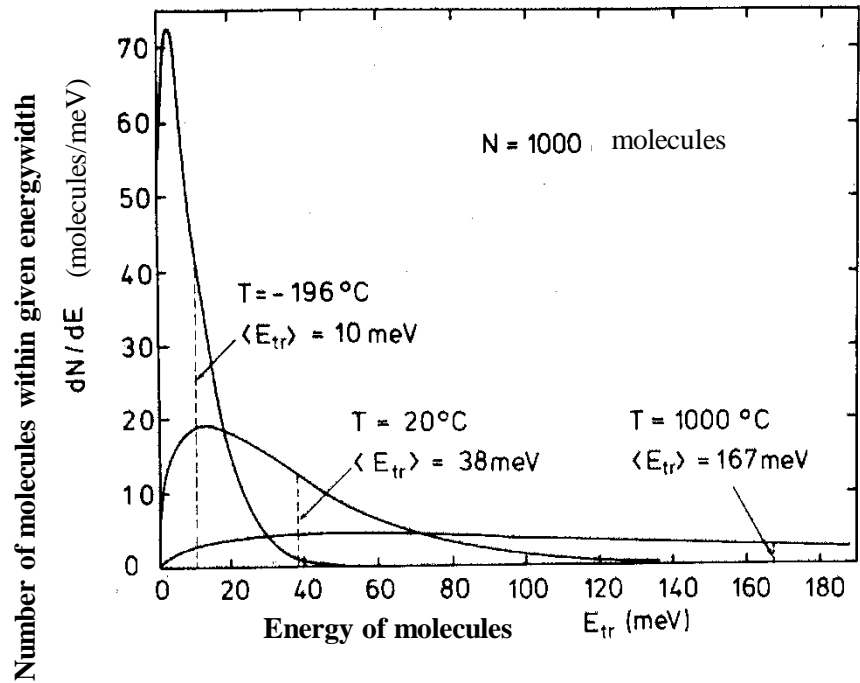
Maxwell-Boltzmann theory:

$$\frac{dN}{dE} = \frac{2 \cdot \pi \cdot N \cdot E^{1/2}}{(\pi \cdot k \cdot T)^{3/2}} \cdot e^{-E/kT}$$

Energy distribution of translation energy

$$\langle E_{tr} \rangle = \frac{3}{2} \cdot k \cdot T$$

Average translation energy of a gas molecule



Translation energy distribution at some temperatures.

Energy

$$U_{tr} = \frac{3}{2} NkT = \frac{3}{2} nRT$$

Translation energy

$$U_{rot} = NkT = nRT$$

Rotation energy (for a 2-atom molecule)

Velocity

$$\frac{dN}{dv} = 4\pi N \left(\frac{m}{2\pi kT} \right)^{3/2} v^2 e^{-\frac{mv^2}{2kT}}$$

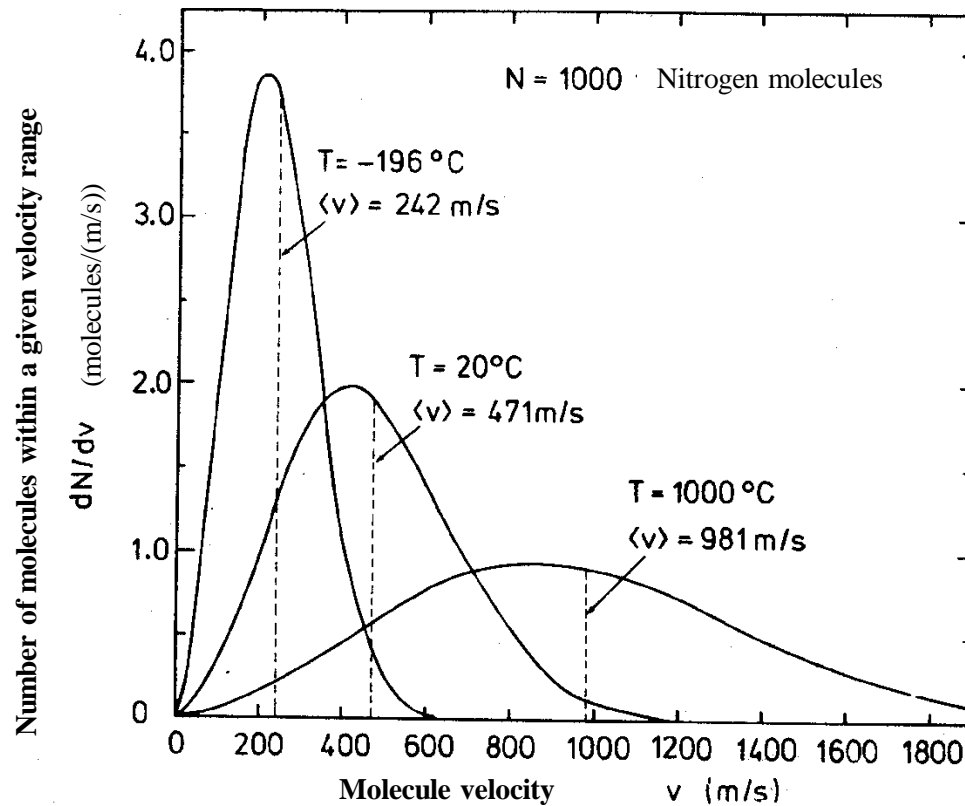
Velocity distribution for gas molecules

$$\langle v \rangle = \left(\frac{8kT}{\pi m} \right)^{1/2}$$

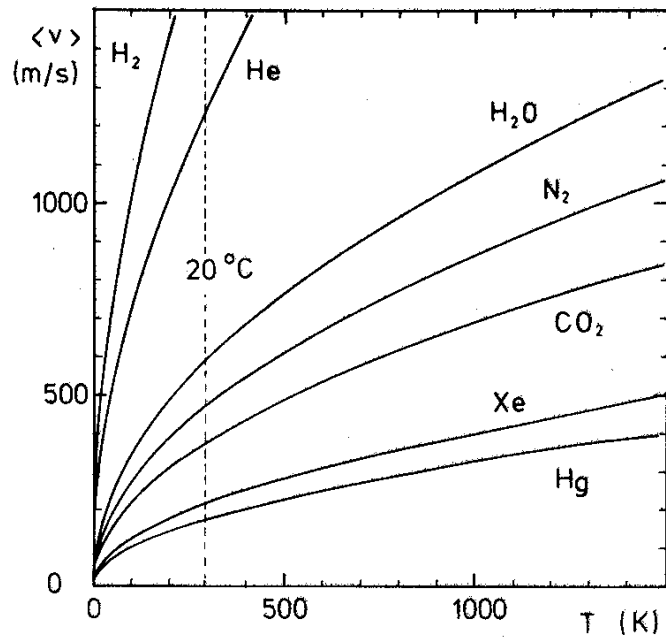
Average velocity

$$v_{prob} = \left(\frac{2kT}{m} \right)^{1/2}$$

Most probable velocity



Velocity distribution of Nitrogen molecules at some temperatures



Application in energy saving windows and thermal insulators: which gas?

Average velocity of some molecules at different temperatures

Molecules on the surface

Molecules of the residual gas stick on the surface

$$\Phi = \frac{P}{(2\pi mkT)^{1/2}}$$

Collision rate on unit area

$$\Phi = \frac{P}{(2\pi mkT)^{1/2}}$$

$$\tau_m = \frac{1}{\xi^2 \Phi}$$

Time for one molecular layer formation

ξ = residual gas molecule diameter

In ultra vacuum, Hydrogen is the dominating gas. At a pressure of 10^{-5} Pa and at 20 °C the molecule layer formation time is

$$\tau_m = \frac{(2\pi\langle\mu\rangle ukT)^{1/2}}{\xi^2 P} =$$

$$\frac{(2\pi \cdot 2.016 \cdot 1.66 \cdot 10^{-27} \text{ kg} \cdot 1.38 \cdot 10^{-23} \text{ J / K} \cdot 293 \text{ K})^{1/2}}{(2.68 \cdot 10^{-10} \text{ m})^2 \cdot 10^{-5} \text{ N / m}} = 12.8 \text{ s}$$

Collision distance

We get also from the M-B distribution for the average collision distance or mean free path:

$$\langle \lambda \rangle = \frac{kT}{\pi \sqrt{2} P \xi^2}$$

For a Nitrogen molecule at 20 °C and 100 kPa

$$\langle \lambda \rangle = 64 \text{ nm}$$

Pressure [Pa]	Collision distance
10^{-10}	64000 km
10^{-7}	64 km
10^{-4}	64 m
10^{-1}	64 mm
10^2	64 μm
10^5	64 nm

Residual gas (N) collision distances at 20 °C

If a fast electron, ion or molecule moves in a residual gas the residual gas molecules can be considered to be at rest. This leads to

$$\langle \lambda \rangle = \frac{kT}{\pi P \xi^2} = \sqrt{2} \langle \lambda \rangle$$

Fast particle

$$\langle \lambda_e \rangle = 4\sqrt{2} \langle \lambda \rangle$$

Electron

So, the mean free path for an accelerated ion at 10^{-5} Pa = 10^{-7} mbar is 905 m

This was the criterion for JYFL vacuum level!

Vacuum criteria

- For beam transport and accelerators:
 - Mean free path = trajectory length
 - Decay time due to collisions
- For “clean” manufacturing (crystal growth, surface manipulation, electronics):
 - Time for building a molecular layer
- What else?

Vacuum pumps

Capacity of a vacuum pump

$$S = \frac{dV}{dt} \quad \text{Pumping speed}$$

$$Q = P \cdot S \quad \text{Transmission of the pump}$$

Evacuation of a vacuum chamber (without additional sources of gas or vapor)

Rough vacuum

- Estimate the required effective pumping speed S_{eff} to pump the volume V from pressure p to p_{end} in a given pump-down time t .
- Assume constant S_{eff}
- Assume $p_{\text{end}} \ll p$

Then

$$-\frac{dp}{dt} = \frac{S_{\text{eff}}}{V} \cdot p$$

- Start from 1013 mbar at $t = 0$
- p at t is calculated from

$$\int_{1013}^p \frac{dp}{p} = -\frac{S_{\text{eff}}}{V} \cdot t$$

$$\ln \frac{p}{1013} = -\frac{S_{\text{eff}}}{V} \cdot t$$

$$S_{\text{eff}} = \frac{V}{t} \cdot \ln \frac{1013}{p} = \frac{V}{t} \cdot 2.3 \cdot \log \frac{1013}{p}$$

- Introduce a dimensionless factor

$$\sigma = \ln \frac{1013}{p} = 2.3 \cdot \log \frac{1013}{p}$$

Then

$$S_{\text{eff}} = \frac{V}{t} \cdot \sigma$$

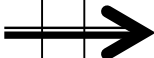
$$t = \tau \cdot \sigma$$

with $\tau = \frac{V}{S_{\text{eff}}}$

and $\sigma = \ln \frac{1013}{p}$

Example

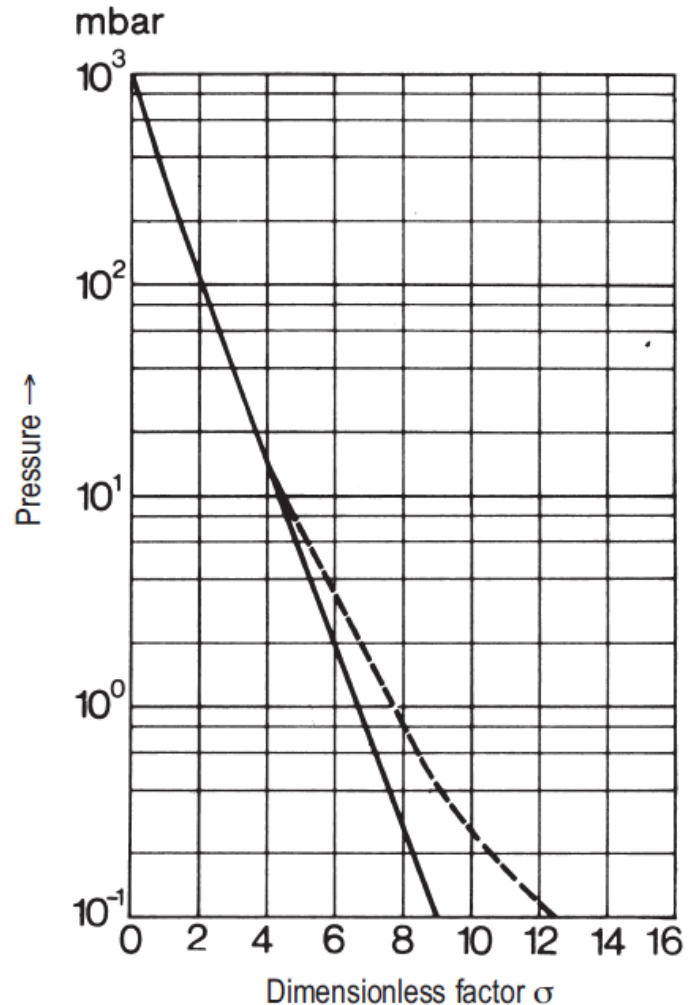
- Volume $V = 500 \text{ l} = 0.5 \text{ m}^3$
- Pumping time to 1 mbar in 10 minutes = $1/6 \text{ h}$


$$\begin{aligned} S_{\text{eff}} &= \frac{0.5}{1/6} \cdot 2.3 \cdot \log \frac{1013}{1} \\ &= 3 \cdot 2.3 \cdot 3.01 = 20.8 \text{ m}^3/\text{h} \end{aligned}$$

- Solid line:
constant pumping
speed
- Dashed line:
pumping speed
reduces below 10
mbar

$$S_{\text{eff}} = \frac{0.5}{\frac{1}{6}} \cdot 7 = 21 \text{ m}^3/\text{h} \quad \text{or}$$

$$S_{\text{eff}} = \frac{0.5}{\frac{1}{6}} \cdot 8 = 24 \text{ m}^3/\text{h}$$



Evacuation of a vacuum chamber with additional sources of gas or vapor

High vacuum region

- Leaks
- Vaporization (e.g. water droplets)
- Outgassing ($mbar \times l \times s^{-1} \times cm^{-2}$)
 - Porous material (epoxy, some plastics, etc.)
 - Molecules on surfaces (eg. water)
- Permeation P ($m^2 \times s^{-1}$)
 - $Q = P \times A \times \Delta p \times d^{-1}$
 - Diffusion through walls
 - Metals $<10^{-14}$
 - Neoprene $10^{-13} - 10^{-11}$
 - Plastics $10^{-12} - 10^{-11}$
 - Viton 10^{-12}
- When the gas evolution Q is known, the effective pumping speed must be at least

$$S_{\text{eff}} = Q/p_{\text{end}}$$

Conductance of the flow channel

$$Q = C \cdot (P_1 - P_2)$$

Q = transmission of the flow channel

P_1 = Pressure at inlet

P_2 = Pressure at outlet

C is called the conductance of the flow channel

$$[C] = m^3/s$$

$$\frac{1}{C} = \text{resistance}$$

$$C = \frac{\pi}{8} d^2 \langle w \rangle \frac{P_1 + P_2}{P_1 - P_2}$$

Conductance for a long round tube in incompressible flow

$$C = \frac{\pi d^4}{256 \eta L} (P_1 + P_2)$$

Conductance for a long round tube in laminar flow

$$C = \frac{1}{6} \left(\frac{2\pi kT}{m} \right)^{1/2} \frac{d^3}{L}$$

Conductance for a long round tube in molecular flow

Note! This does NOT depend on pressure